

Reducing Methane Emissions through Directed Inspection and Maintenance (DI&M)

Oil & Gas Subcommittee Technology Transfer Workshop

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# Directed Inspection and Maintenance and Infrared Leak Detection Agenda

- What are fugitive equipment leaks?
- What is DI&M
- Infrared Leak Detection
- Partner Experience
- Discussion



# **Key Characteristics of Fugitive Equipment Leaks**

- Fugitive equipment leaks are a major source of CH<sub>4</sub> emissions at oil and gas facilities.
- Most of these emissions are from a few big leaks rather than many small or medium sized leaks.
- 75 to 85% of the emissions from leaks are cost effective to fix (often payback of <6 months).</li>
- Components in gas service leak more than those in liquid service.
- Components in sweet service more likely to leak than those in sour or odorized service.
- Leak potential tends to increase with time and usage.
- Different types of components and service applications have different leak potentials (i.e., leak magnitude and probability).
- Components in vibration, cryogenic or thermal cycling service have an increased leak potential.



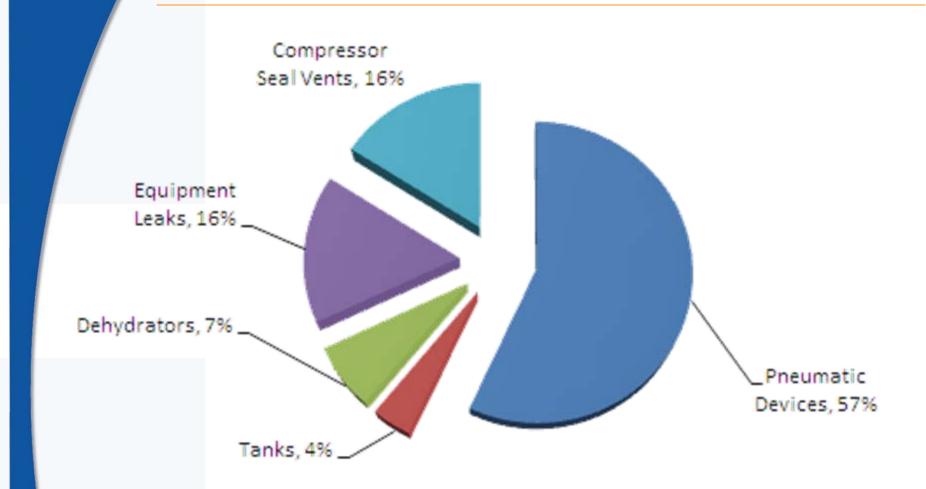
### Why Do Big Leaks Occur?

 Big leaks often go unnoticed because they occur in difficult-to-access, lowtraffic, congested or noisy areas, or the amount of leakage is not fully appreciated.

 Big leaks may also occur because of severe/demanding applications or the high cost or difficulty of repairs.



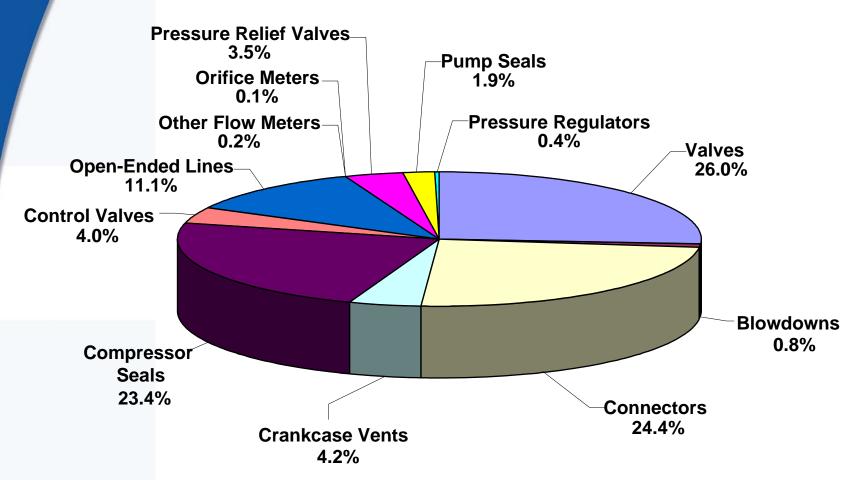
### Methane Emissions at 76 Gas Production Facilities



Source: Clearstone Engineering

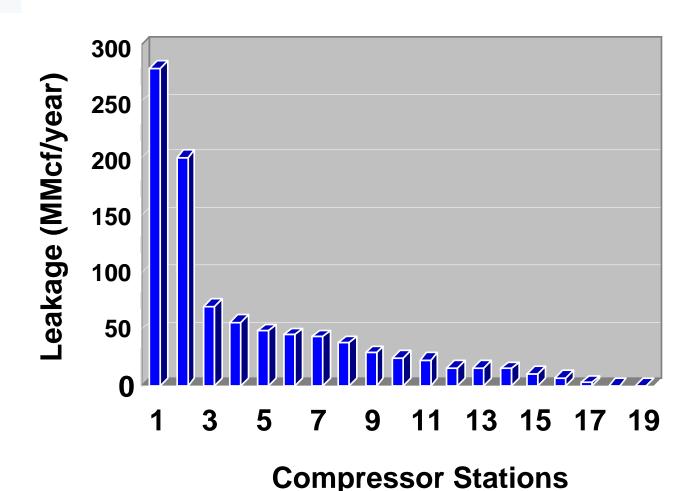


# Distribution of Losses by Type of Component (Processing)





# Measured Leakages in Compressor Stations



Source: Clearstone Engineering, 2002



# What is Normal Leak Control Practice?

- Perform a leak check (using a bubble test or hand-held gas sensor) on equipment components when first installed, and after inspection & maintenance.
- Thereafter, leaks are detected by:
  - Area or building monitors.
  - Personal monitors.
  - Olfactory, audible or visual indicators.
- Leaks only fixed if this is easy to do or they pose an obvious safety concern.
- Unmanned facilities get less attention than manned facilities.
- Priority following a facility turnaround is to get it back on line rather than ensure all affected components have been leak checked.



# What is Directed Inspection & Maintenance (DI&M)?

It is a practicable ongoing approach to achieving significant cost-effective reductions in fugitive equipment leaks:

- Find the big leaks in an efficient manner:
  - Focus efforts on the most likely sources of big leaks with coarse or less frequent screening of other components.
- Only repair components that are cost-effective to repair or pose a safety or environmental concern.
- Minimize the potential for big leaks and provide early detection and repair of these when they occur.



#### What are the benefits of DI&M?

- Attractive payback (often <6 months).</li>
- Reduced maintenance costs.
- Reduced downtime.
- Improved process efficiency.
- Safer work environment.
- Cleaner environment.
- Resource conservation.



### Where Should Leak Monitoring **Efforts Be Focused?**

| Table 1. Sample leak statistics for gas transmission facilities. |                      |                   |                                       |                                       |   |                               |  |
|--|----------------------|-------------------|---------------------------------------|---------------------------------------|---|-------------------------------|--|
| Source   | Number of<br>Sources | Leak<br>Frequency | Average<br>Emissions<br>(lb/h/source) | Percent of<br>Component<br>Population | Contribution to<br>Total Emissions<br>(%) | Relative<br>Leak<br>Potential |  |
| Station or Pressurized<br>Blowdown System                        | 219                  | 59.8              | 7.50E+00                              | 0.131                                 | 53.170                                    | 7,616.00                      |  |
| Compressor Seal –<br>Centrifugal                                 | 103                  | 64.1              | 2.79E+00                              | 0.061                                 | 9.313                                     | 2,838.00                      |  |
| Compressor Seal –<br>Reciprocating                               | 167                  | 40.1              | 2.35E+00                              | 0.099                                 | 12.722                                    | 2,400.00                      |  |
| Pressure Relief Valve  | 612                  | 31.2              | 3.56E-01                              | 0.366                                 | 7.058                                     | 362.00                        |  |
| Open-Ended Line  | 928                  | 58.1              | 2.02E-01                              | 0.555                                 | 6.065                                     | 205.00                        |  |
| Orifice Meter  | 185                  | 22.7              | 1.07E-01                              | 0.110                                 | 0.640                                     | 109.00                        |  |
| Control Valve  | 782                  | 9.0               | 3.63E-02                              | 0.467                                 | 0.918                                     | 37.00                         |  |
| Pressure Regulator   | 816                  | 7.0               | 1.75E-02                              | 0.488                                 | 0.461                                     | 18.00                         |  |
| Valve  | 17,029               | 2.8               | 9.09E-03                              | 10.190                                | 5.007                                     | 9.00                          |  |
| Connector  | 145,829              | 0.9               | 9.83E-04                              | 87.263                                | 4.641                                     | 1.00                          |  |
| Other Flow Meter   | 443                  | 1.8               | 2.19E-05                              | 0.265                                 | 0.0003                                    | 0.02                          |  |

2.19E-05

1.8

Source: Clearstone Engineering, 2007

0.02

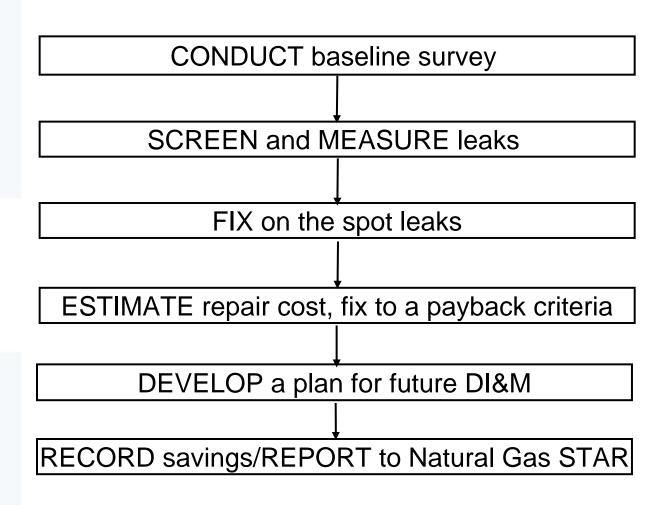


# How Frequently Should Components Be Monitored?

| Suggested leak monitoring frequencies for equipment components, |                      |                |                 |                   |  |  |
|---|----------------------|----------------|-----------------|-------------------|--|--|
| presented by component category and type.                       |                      |                |                 |                   |  |  |
| Source  | Type of              | Service        | Application     | Frequency         |  |  |
| Category  | Component            |                |                 |                   |  |  |
| Process Equipment   | Connectors and       | All            |                 | Immediately after |  |  |
|   | Covers               |                |                 | any adjustments   |  |  |
|   |                      |                |                 | and once every 5  |  |  |
|   |                      |                |                 | years thereafter  |  |  |
|   |                      | All            | Thermal Cycling | Bi-annually       |  |  |
|   |                      | All            | Vibration       | Annually          |  |  |
|   | Control Valves       | Gas/Vapour/LPG |                 | Annually          |  |  |
|   |                      | Gas/Vapour/LPG | Thermal Cycling | Bi-annually       |  |  |
|   | Block Valves –       | Gas/Vapour/LPG | All             | Annually          |  |  |
|   | Rising Stem          |                |                 |                   |  |  |
|   | Block Valves –       | Gas/Vapour/LPG | All             | Once every 5      |  |  |
|   | Quarter Turn         |                |                 | years             |  |  |
|   | Compressor Seals     | All            | All             | Monthly           |  |  |
|   | Pump Seals           | All            | All             | Quarterly         |  |  |
|   | Pressure Relief      | All            | All             | Annually          |  |  |
|   | Valves               |                |                 |                   |  |  |
|   | Open-ended Lines     | All            | All             | Annually          |  |  |
|   | Emergency Vent       | All            | All             | Quarterly         |  |  |
|   | and Blowdown         |                |                 |                   |  |  |
|   | Systems <sup>1</sup> |                |                 |                   |  |  |
| Vapour Collection   | Tank Hatches         | All            | All             | Monthly           |  |  |
| Systems   | Pressure-Vacuum      | All            | All             | Monthly           |  |  |
|   | Safety Valves        |                |                 |                   |  |  |

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#### Screening - find the leaks

- Soap bubble screening
- Electronic screening ("sniffer")
- Toxic vapor analyzer (TVA)
- Organic vapor analyzer (OVA)
- Ultrasound leak detection
- Acoustic leak detection
- Infrared leak detection







- Evaluate the leaks detected measure results
  - High volume sampler
  - End-of-pipe technologies
    - Velocity traverse
    - Rotameters
    - Calibrated bagging
  - Toxic vapor analyzer (correlation factors)

Leak Measurement Using High Volume Sampler





| Summary of Screening and Measurement Techniques |               |                          |  |  |
|---|---------------|--------------------------|--|--|
| Instrument/ Technique                           | Effectiveness | Approximate Capital Cost |  |  |
| Soap Solution                                   | **            | \$                       |  |  |
| Electronic Gas Detector                         | *             | \$\$                     |  |  |
| Acoustic Detector/ Ultrasound Detector          | **            | \$\$\$                   |  |  |
| TVA (Flame Ionization Detector)                 | *             | \$\$\$                   |  |  |
| Calibrated Bagging                              | *             | \$\$                     |  |  |
| High Volume Sampler                             | ***           | \$\$\$                   |  |  |
| End-of-pipe Flow Measurement                    | **            | \$\$                     |  |  |
| Infrared Leak Detection                         | ***           | \$\$\$\$                 |  |  |
| Source: EPA's Lessons Learned                   | •             |                          |  |  |

<sup>\* -</sup> Least effective at screening/measurement

<sup>\$ -</sup> Smallest capital cost

<sup>\*\*\* -</sup> Most effective at screening/measurement

<sup>\$\$\$ -</sup> Largest capital cost



# **Estimating Comprehensive Leak Survey Costs**

- Cost of complete screening survey using high volume sampler (processing plant)
  - Ranges US\$15,000 to US\$20,000 per medium-size plant
  - Rule of Thumb: US\$1 per component for an average processing plant
  - Cost per component for remote production sites would be higher than US\$1
- 25 to 40% cost reduction for follow-up survey
  - Focus on higher probability leak sources (e.g. compressors)



### **DI&M** by Infrared Leak Detection

## Real-time detection of methane leaks

- Quicker identification of leaks.
- Screen hundreds of components an hour.
- Screen inaccessible areas
  simply by viewing them.

#### Infrared Leak Detection



Source: Leak Surveys Inc.



Source: Heath Consultants



#### **Infrared Methane Leak Detection**

Video recording of fugitive leaks detected by various infrared devices





### **Is Recovery Profitable?**

| Repair the Cost-Effective Components |                           |                              |                     |  |  |  |
|--------------------------------------|---------------------------|------------------------------|---------------------|--|--|--|
| Component                            | Value of lost gas¹ (US\$) | Estimated repair cost (US\$) | Payback<br>(months) |  |  |  |
| Plug Valve: Valve Body               | 21,070                    | 200                          | 0.11                |  |  |  |
| Union: Fuel Gas Line                 | 20,260                    | 100                          | 0.06                |  |  |  |
| Threaded Connection                  | 17,410                    | 10                           | 0.01                |  |  |  |
| Distance Piece: Rod Packing          | 12,750                    | 2,000                        | 1.88                |  |  |  |
| Open-Ended Line                      | 11,600                    | 60                           | 0.06                |  |  |  |
| Compressor Seals                     | 9,640                     | 2,000                        | 2.49                |  |  |  |
| Gate Valve                           | 7,880                     | 60                           | 0.09                |  |  |  |

Source: Hydrocarbon Processing, May 2002 (Repair cost)

1 – Adjusted to US\$5/MMBtu gas price



#### **DI&M - Lessons Learned**

- A successful, cost-effective DI&M program requires measurement of the leaks
- A high volume sampler is an effective tool for quantifying leaks and identifying cost-effective repairs
- Open-ended lines, compressor seals, blowdown valves, engine-starters, and pressure relief valves represent <3% of components but >60% of methane emissions
- The business of leak detection has changed dramatically with new technology



Source: Chevron



#### **Discussion**

- Industry experience applying these technologies and practices
- Limitations on application of these technologies and practices
- Actual costs and benefits