



G L O B A L F O R U M

On Flaring and Venting Reduction  
and Natural Gas Utilisation

# Synfuels International, Inc. Upstream GTL Solutions for Flaring



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*Chief Engineer*

# Why Synfuels pursued an economical GTL & GTE process

- **Government restrictions on flaring**
- **Global Environmental concerns**
- **Increasing demand for 'transportable' liquid fuel in emerging economies**
- **Laws favouring cleaner fuels**
- **Need for greater utilization of resources**
- **Rising energy prices**

# Fischer-Tropsch (F-T)

## *Limitations*

- F-T needs huge plants to create the necessary economies of scale
- F-T's minimum economic size is about 300 MMSCFD
- Primary F-T product has wide molecular weight distribution – lots of waxes and light ends
- Of 15,000+ gas fields outside North America's pipeline network, less than 200 can support mega-scale F-T plants

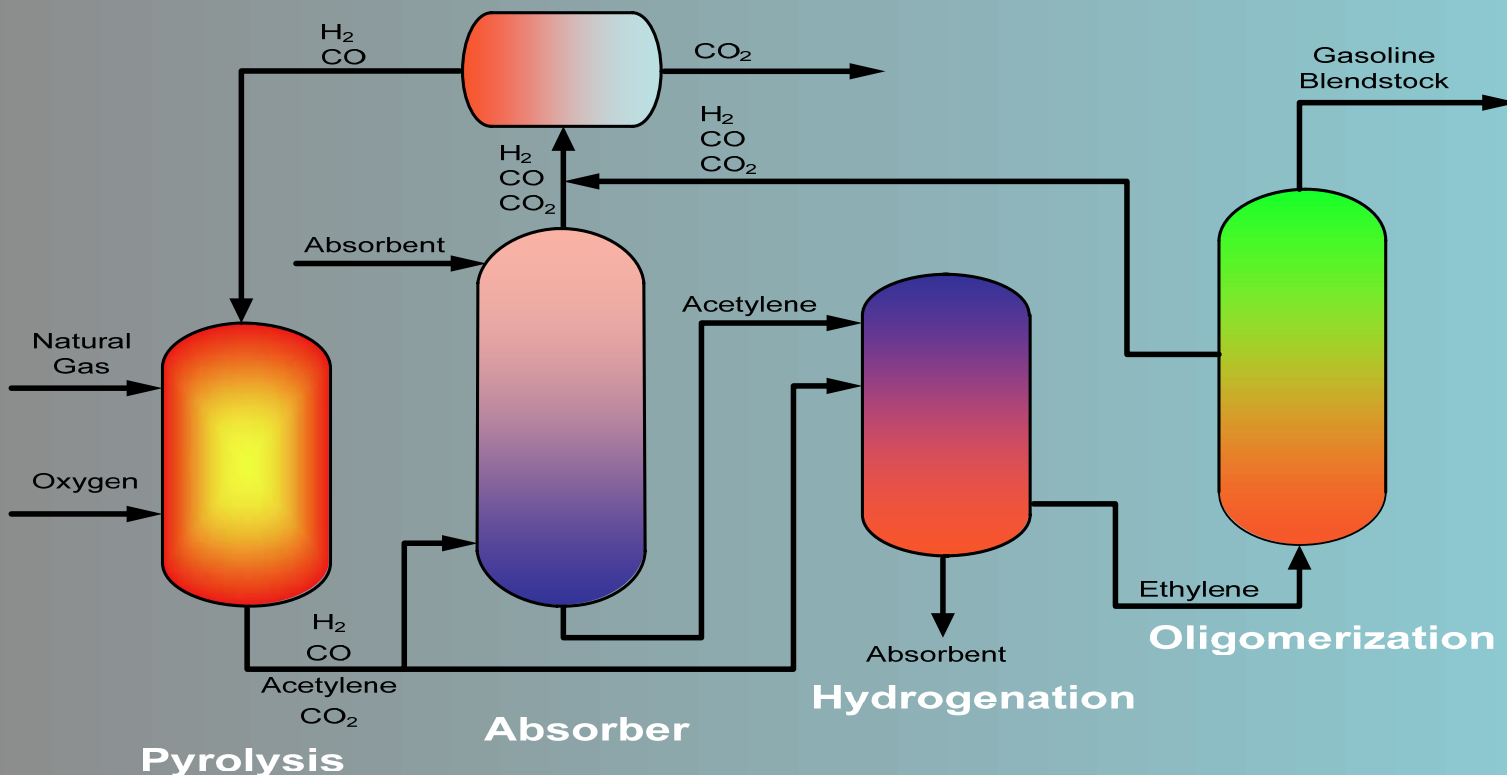
***“Smaller fields need smaller plants that require much less capital than Fischer-Tropsch demands.”***

# NEW

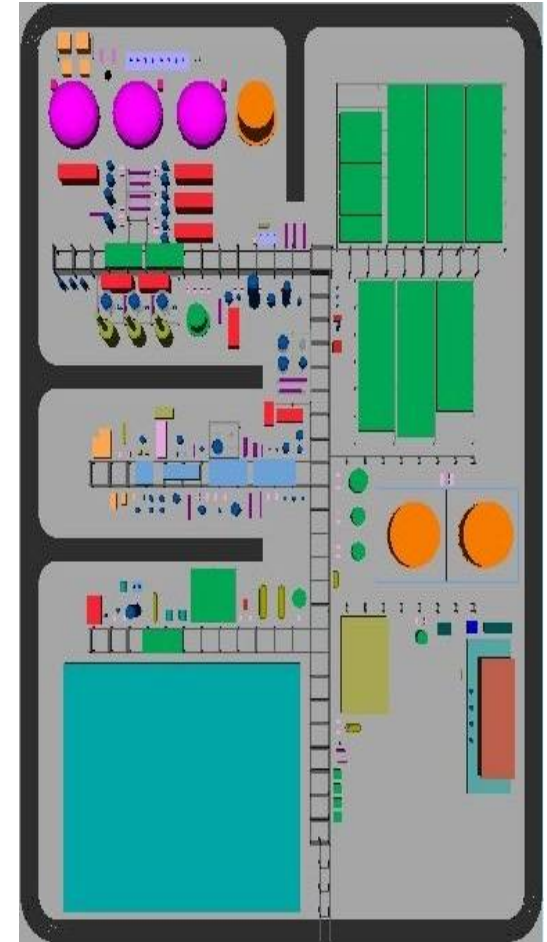


- Innovative new approach – Not a F-T modification
- Lower operating pressure than F-T. Therefore, lower cost and easier fabrication
- Near 0% recycled gas. This reduces operating costs
- Demonstrated effective down to 30 MSCFD
- Most economical between 10 and 250 MMSCFD

## Synfuels International GTE/GTL Technology



# 50 MMSCFD Plant Design



# Clean Gasoline from Methane

## Synfuels GTL Product Properties

<b>Specific Gravity</b>	<b>0.7599 (Water=1)</b>
<b>°API Gravity</b>	<b>54.71 @ 60°F</b>
<b>Molecular Weight</b>	<b>100.422</b>
<b>Weight</b>	<b>6.33 Lbs/Gal</b>
<b>Gross Heating Value</b>	<b>124190 BTU/CF</b>

## Synfuels GTL Product Composition

	<b>vol%</b>
<b>Paraffins</b>	<b>12</b>
<b>Iso-paraffins</b>	<b>35.9</b>
<b>Olefins</b>	<b>1</b>
<b>Naphthenes</b>	<b>9.8</b>
<b>Aromatics</b>	<b>38.5</b>

# Gas-Phase Hydrogenation Problems

- Must limit acetylene concentration for reaction and temperature control
- High temperature can lead to a “run-away” reaction
- Requires processing large volumes of diluents rich gas
- Tends toward over-conversion to ethane

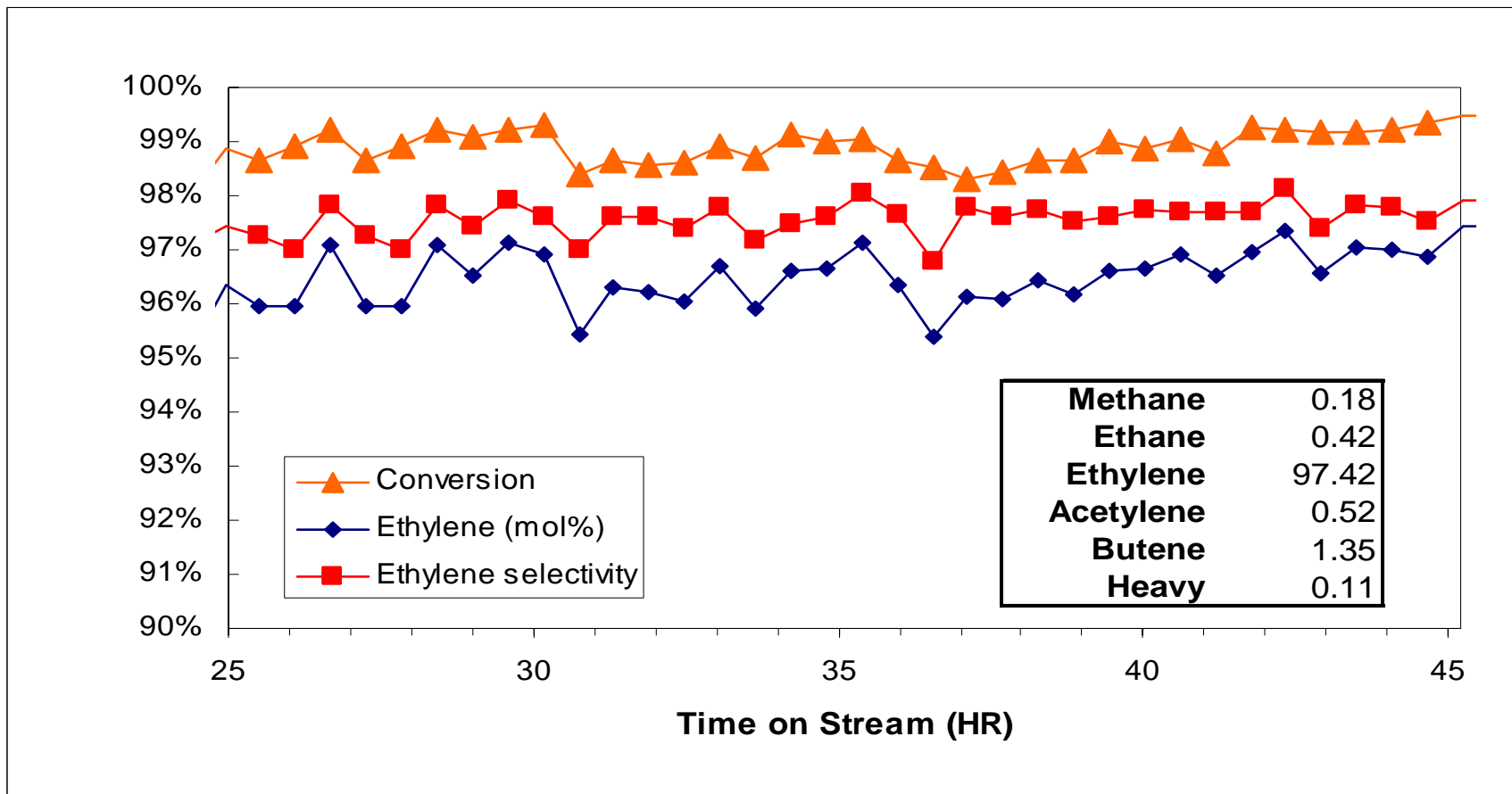


# Synfuels Uses Liquid-Phase Hydrogenation of Acetylene

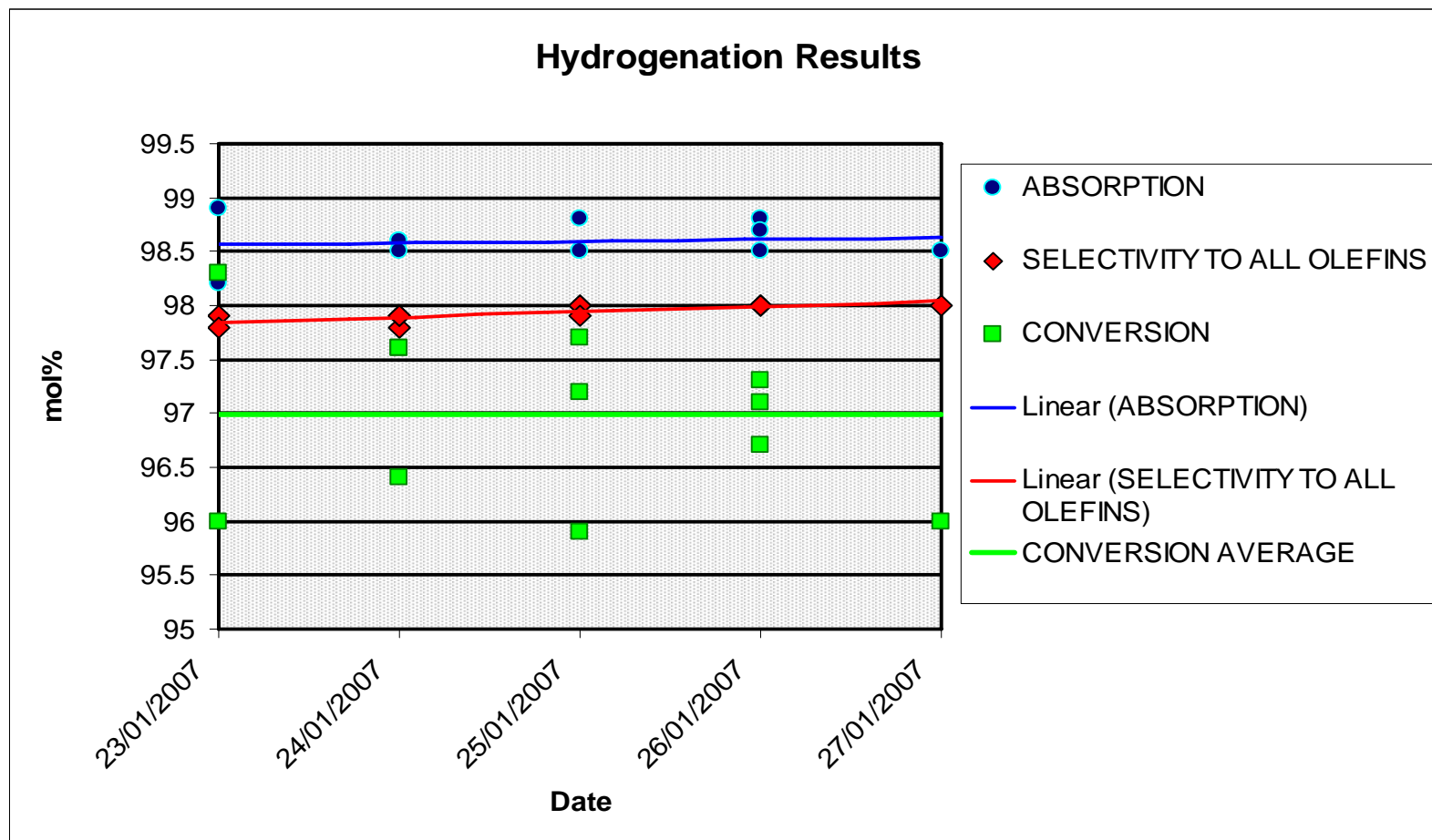
- Selectively absorbs acetylene
- Rejects unwanted gases
- Greatly reduces volume of processed gas
- Operates at moderate conditions
- No thermal “run-away” reaction
- Much higher acetylene concentrations can be used

# Extended Duration Conversion and Selectivity

Lab Data



# Plant Results



# Intellectual Property

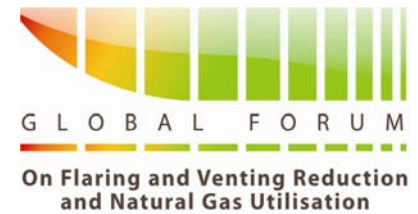
Synfuels Technology is covered by 10 US Patents and dozens of patents pending:

<u>Method for Converting Natural Gas to Liquid Hydrocarbons</u>	Patent Number:6,130,260
<u>Method for Converting Natural Gas to Liquid Hydrocarbons</u>	Patent Number:6,323,247
<u>Method for Converting Methane-Containing Gaseous Hydrocarbon Mixtures to Liquid Hydrocarbons</u>	Patent Number:6,433,235
<u>Method for Converting Natural Gas to Liquid Hydrocarbons</u>	Patent Number:6,602,920
<u>Process for Liquid Phase Hydrogenation</u>	Patent Number:7,045,670
<u>Method for Converting Natural Gas to Olefins</u>	Patent Number:7,119,240
<u>Process for Conversion of Natural Gas to Hydrocarbon Liquids</u>	Patent Number:7,183,451
<u>Process for Conversion of Natural Gas to Ethylene</u>	Patent Number:7,208,647
<u>High Temperature Hydrocarbon Cracking</u>	Patent Number:7,250,449
<u>Process for Liquid Phase Hydrogenation</u>	Patent Number:7,408,091

# Summary

- A unique, patented natural gas to gasoline or ethylene process
- Established, fully scalable, industrially proven design
- Synfuels liquid-phase hydrogenation is the technology's cornerstone
- Breakthrough technology reduces recycle, compression and system volumes resulting in low capital and operating cost and High IRR
- **Flaring problems eliminated with Synfuels Gas-to-Gasoline plants erected up-stream, on-site**

# Synfuels Top Team



## **Synfuels International, Inc.**

Mr. Ben Weber, CEO

Mr. Thomas Rolfe, President

Mr. Charles Matar, Managing Director, MENA

Dr. Ed Peterson, Chief Engineer

## **Bryan Research and Engineering**

Prof. Jerry Bullin, President

Dr. Joel Cantrell, Development Engineer

## **Texas A&M University**

Prof. Kenneth Hall, former Head of Chemical Engineering